

Rising Bubble

This example shows how to model two immiscible fluids, tracking the fluid-fluid interface. An oil bubble rises through water and merges with oil already residing at the top of the container. Initially three different regions exist: the initially still oil bubble, the oil at the top of the container, and the water surrounding the bubble (see Figure 1). The container is cylindrical with a diameter of 1.10^{-2} m and a height of $1.5.10^{-2}$ m. The oil phase has a viscosity of 0.0208 Pa·s and has a density of 879 kg/m³. For water the viscosity is $1.01 \cdot 10^{-3}$ Pa·s and the density is 998.2 kg/m³. Buoyancy effects cause the oil bubble to rise through the water phase. As the bubble reaches the liquid-liquid interface, it merges with the oil phase.

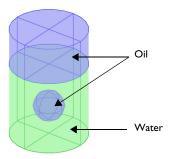


Figure 1: Initial bubble position. The geometry is axisymmetric.

As outlined above, the topology of the fluid interface changes with time. You start with three separate fluid regions and end up with two. The level set method as well as the phase field method are both well suited for modeling moving boundaries where topology changes occur. Both methods are available in the CFD Module as predefined multiphysics interfaces. This example shows you how to use the Laminar Two-Phase Flow, Level Set interface.

Model Definition

REPRESENTATION AND CONVECTION OF THE FLUID INTERFACE

The Level Set interface finds the fluid interface by tracing the isolines of the level set function, ϕ . The level set or isocontour $\phi = 0.5$ determines the position of the interface. The equation governing the transport and reinitialization of ϕ is

$$\frac{\partial \phi}{\partial t} + \mathbf{u} \cdot \nabla \phi = \gamma \nabla \cdot \left(\varepsilon \nabla \phi - \phi (1 - \phi) \frac{\nabla \phi}{|\nabla \phi|} \right)$$

where \mathbf{u} (SI unit: m/s) is the fluid velocity, and γ (SI unit: m/s) and ε (SI unit: m) are reinitialization parameters. The ε parameter determines the thickness of the layer around the interface where ϕ goes from zero to one. When stabilization is used for the level set equation, you can typically use an interface thickness of $\varepsilon = h_c/2$, where h_c is the characteristic mesh size in the region passed by the interface. The γ parameter determines the amount of reinitialization. A suitable value for γ is the maximum velocity magnitude occurring in the model.

Because the level set function is a smooth step function, it is also used to determine the density and dynamic viscosity globally by

$$\rho = \rho_w + (\rho_o - \rho_w)\phi$$

and

$$\mu = \mu_w + (\mu_o - \mu_w)\phi$$

Here ρ_w , μ_w , ρ_o , and μ_o denote the constant density and viscosity of water and oil, respectively.

MASS AND MOMENTUM TRANSPORT

In the Laminar Two-Phase Flow, Level Set interface, the transport of mass and momentum is governed by the incompressible Navier-Stokes equations, including surface tension:

$$\rho \left(\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right) = -\nabla p + \nabla \cdot \mu (\nabla \mathbf{u} + \nabla \mathbf{u}^T) + \rho \mathbf{g} + \mathbf{F}_{st}$$
$$\nabla \cdot \mathbf{u} = 0$$

In the above equations, ρ (SI unit: kg/m³) denotes the density, **u** is the velocity (SI unit: m/s), t equals time (SI unit: s), p is the pressure (SI unit: Pa), and μ denotes the viscosity (SI unit: Pa·s). The momentum equations contain gravity, ρ **g**, and surface tension force components, denoted by **F**_{st}.

Surface Tension

The surface tension force is defined by

$$\mathbf{F}_{et} = \nabla \cdot \mathbf{T} = \nabla \cdot [\sigma \{ \mathbf{I} + (-\mathbf{n}\mathbf{n}^T) \} \delta]$$

where σ is the surface tension coefficient, **I** is the identity matrix, **n** is the interface unit normal, and δ is a Dirac delta function, nonzero only at the fluid interface. The interface normal is calculated from

$$\mathbf{n} = \frac{\nabla \phi}{|\nabla \phi|}$$

The level set parameter ϕ is also used to approximate the delta function by a smooth function defined by

$$\delta = 6|\phi(1-\phi)||\nabla\phi|$$

INITIAL CONDITION

At t = 0, the velocity is zero. Figure 2 shows the initial level set function. This is automatically computed using a Phase Initialization study step by solving for the geometrical distance to the initial interface, D_{wi} . The initialized level set function is then defined from the analytical steady state solution for a straight fluid-fluid interface:

$$\phi_{1,0} = \frac{1}{1 + e^{D_{\text{wi}}/\epsilon}}, \quad \phi_{2,0} = \frac{1}{1 + e^{-D_{\text{wi}}/\epsilon}},$$

in the domains initially filled with Fluid 1 and Fluid 2 respectively,



Figure 2: A surface and contour plot of the initialized level set function.

BOUNDARY CONDITIONS

Use no slip conditions, $\mathbf{u} = 0$ at the top and bottom and a wetted wall condition on the right boundary. The left boundary corresponds to the symmetry axis.

Figure 3 and Figure 4 contain snapshots of the fluid interface. The snapshots show how the bubble travels up through the water and merges with the oil above. As the bubble rises, its shape remains spherical due to the surface tension and the high viscosity of the oil. As the droplet hits the water surface, it merges with the oil above and creates waves on the surface.

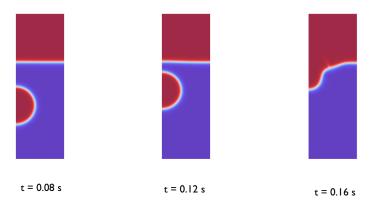


Figure 3: Snapshots showing the interface prior to and just after the bubble hits the surface.

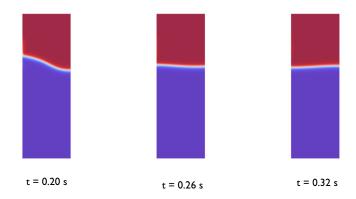


Figure 4: Snapshots showing the interface after the bubble has merged with the oil above.

One way to investigate the quality of the numerical results is to check the conservation of mass. Because there are no reactions and no flow through the boundaries, the total mass of each fluid should be constant in time. Figure 5 shows the total mass of oil as a function of time. The mass loss during simulation is small, showing that the model conserves mass.

Exact mass conservation is obtained when using the conservative level set form. However, the conservative form is less suited for numerical calculations and convergence is harder.

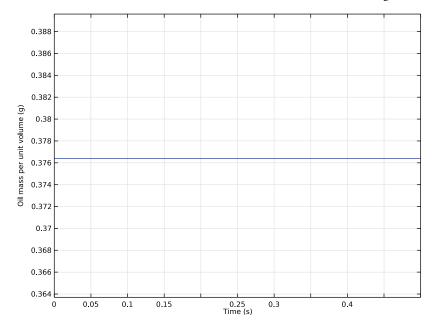


Figure 5: Total mass of oil as a function of time. The total mass loss during the simulation is conserved.

Notes About the COMSOL Implementation

The model is straightforward to set up and solve using either the Laminar Two-Phase Flow, Level Set interface. Automatically, two study steps are created. The first one initializes the level set function, and the second one calculates the dynamic two phase flow problem.

Application Library path: CFD_Module/Multiphase_Flow/rising_bubble_2daxi

Modeling Instructions

From the File menu, choose New.

NEW

In the New window, click Model Wizard.

MODEL WIZARD

- I In the Model Wizard window, click 2D Axisymmetric.
- 2 In the Select Physics tree, select Fluid Flow>Multiphase Flow>Two-Phase Flow, Level Set> Laminar Flow.
- 3 Click Add.
- 4 Click 🔵 Study.
- 5 In the Select Study tree, select Preset Studies for Selected Multiphysics>
 Time Dependent with Phase Initialization.
- 6 Click M Done.

GEOMETRY I

- I In the Model Builder window, under Component I (compl) click Geometry I.
- 2 In the Settings window for Geometry, locate the Units section.
- 3 From the Length unit list, choose mm.

Rectangle I (rI)

- I In the Geometry toolbar, click Rectangle.
- 2 In the Settings window for Rectangle, locate the Size and Shape section.
- 3 In the Width text field, type 5.
- 4 In the **Height** text field, type 15.
- 5 Click **Pauld Selected**.

Polygon I (poll)

- I In the Geometry toolbar, click / Polygon.
- 2 In the Settings window for Polygon, locate the Coordinates section.
- **3** From the **Data source** list, choose **Vectors**.
- 4 In the r text field, type 0 5.
- 5 In the z text field, type 10.
- 6 Click Pauld Selected.

Circle I (c1)

- I In the Geometry toolbar, click Circle.
- 2 In the Settings window for Circle, locate the Size and Shape section.

- 3 In the Radius text field, type 2.
- 4 In the Sector angle text field, type 180.
- **5** Locate the **Position** section. In the **z** text field, type 4.
- 6 Locate the Rotation Angle section. In the Rotation text field, type -90.
- 7 Click **P** Build Selected.

Form Union (fin)

- I In the Model Builder window, click Form Union (fin).
- 2 In the Settings window for Form Union/Assembly, click | Build Selected.

MULTIPHYSICS

Two-Phase Flow, Level Set I (tpfl)

- I In the Model Builder window, under Component I (compl)>Multiphysics click Two-Phase Flow, Level Set I (tpfl).
- 2 In the Settings window for Two-Phase Flow, Level Set, locate the Material Properties section.
- 3 Click Add Multiphase Material.
- 4 Locate the Surface Tension section. Select the Include surface tension force in momentum equation check box.
- 5 From the Surface tension coefficient list, choose Library coefficient, liquid/liquid interface.
- 6 From the list, choose Olive oil/Water, 20°C.

MATERIALS

Phase I (mpmat1.phase1)

- I In the Model Builder window, under Component I (compl)>Materials> Multiphase Material I (mpmatl) click Phase I (mpmatl.phaseI).
- 2 In the Settings window for Phase, locate the Link Settings section.
- 3 Click Radd Material from Library . This button is found when expanding the options next to the Material list.

ADD MATERIAL TO PHASE I (MPMATI.PHASEI)

- I Go to the Add Material to Phase I (mpmat1.phaseI) window.
- 2 In the tree, select Liquids and Gases>Liquids>Transformer oil.
- 3 Click OK.

MATERIALS

Phase 2 (mpmat1.phase2)

- I In the Model Builder window, under Component I (compl)>Materials> Multiphase Material I (mpmatl) click Phase 2 (mpmatl.phase2).
- 2 In the Settings window for Phase, locate the Link Settings section.
- 3 Click Add Material from Library. This button is found when expanding the options next to the Material list.

ADD MATERIAL TO PHASE 2 (MPMATI.PHASE2)

- I Go to the Add Material to Phase 2 (mpmat1.phase2) window.
- 2 In the tree, select Liquids and Gases>Liquids>Water.
- 3 Click OK.

LEVEL SET (LS)

Level Set Model 1

- I In the Model Builder window, under Component I (compl)>Level Set (Is) click Level Set Model I.
- 2 In the Settings window for Level Set Model, locate the Level Set Model section.
- **3** In the γ text field, type 0.2.

Initial Values, Fluid 2

- I In the Model Builder window, click Initial Values, Fluid 2.
- **2** Select Domain 1 only.

LAMINAR FLOW (SPF)

- I In the Model Builder window, under Component I (compl) click Laminar Flow (spf).
- 2 In the Settings window for Laminar Flow, locate the Physical Model section.
- 3 Select the **Include gravity** check box.

Pressure Point Constraint I

- I In the Physics toolbar, click Points and choose Pressure Point Constraint.
- 2 Select Point 8 only.

MULTIPHYSICS

Wetted Wall I (ww1)

- I In the Model Builder window, under Component I (compl)>Multiphysics click Wetted Wall I (wwI).
- 2 Select Boundaries 9 and 10 only.

Before creating the mesh, add a variable for computing the mass of oil in the model domain. You will use this variable later to test mass conservation.

DEFINITIONS

Variables 1

- I In the Home toolbar, click a= Variables and choose Local Variables.
- 2 In the Settings window for Variables, locate the Variables section.
- **3** In the table, enter the following settings:

Name	Expression	Unit	Description
rho_oil	tpf1.rho1*tpf1.Vf1	kg/m³	Oil mass per unit volume

MESH I

Free Triangular 1

In the Mesh toolbar, click Free Triangular.

Size

- I In the Model Builder window, click Size.
- 2 In the Settings window for Size, locate the Element Size section.
- 3 From the Calibrate for list, choose Fluid dynamics.
- 4 From the Predefined list, choose Finer.
- 5 Click III Build All.

STUDY I

Step 2: Time Dependent

- I In the Model Builder window, under Study I click Step 2: Time Dependent.
- 2 In the Settings window for Time Dependent, locate the Study Settings section.
- 3 In the Output times text field, type range (0,0.5/50,0.5).

Solution I (soll)

- I In the Study toolbar, click Show Default Solver.
- 2 In the Settings window for Solution, click **Compute**.

RESULTS

Next, test to what degree the total mass of oil is conserved.

Surface Integration I

- I In the Results toolbar, click 8.85 More Derived Values and choose Integration>
 Surface Integration.
- 2 In the Settings window for Surface Integration, locate the Selection section.
- 3 From the Selection list, choose All domains.
- 4 Click Replace Expression in the upper-right corner of the Expressions section. From the menu, choose Component I (compl)>Definitions>Variables>rho_oil Oil mass per unit volume kg/m³.
- **5** Locate the **Expressions** section. In the table, enter the following settings:

Expression	Unit	Description	
rho_oil	g	Oil mass per unit volume	

6 Click **= Evaluate**.

TABLE

- I Go to the Table window.
- 2 Click Table Graph in the window toolbar.

RESULTS

ID Plot Group 6

- I In the Model Builder window, under Results click ID Plot Group 6.
- 2 In the Settings window for ID Plot Group, locate the Axis section.
- 3 Select the Manual axis limits check box.
- **4** In the **x minimum** text field, type **0**.
- 5 In the x maximum text field, type 0.5.
- 6 In the y minimum text field, type 0.3637.
- 7 In the y maximum text field, type 0.3896.

Compare the result to that in Figure 5. As the plot shows, mass is conserved.

Volume Fraction of Fluid 1 (Is)

- I In the Model Builder window, click Volume Fraction of Fluid I (Is).
- 2 In the Settings window for 2D Plot Group, locate the Plot Settings section.
- 3 Clear the Plot dataset edges check box.

Surface I

- I In the Model Builder window, expand the Volume Fraction of Fluid I (Is) node, then click Surface 1.
- 2 In the Settings window for Surface, locate the Coloring and Style section.
- Change Color Table.
- 4 In the Color Table dialog box, select Wave>WaveLight in the tree.
- 5 Click OK.

Volume Fraction of Fluid 1 (Is)

To reproduce the plots in Figure 2 and Figure 3, plot the solution for the time values 0 0.08 0.12, 0.16, 0.20, 0.26, and 0.32.

- I In the Model Builder window, click Volume Fraction of Fluid I (Is).
- 2 In the Settings window for 2D Plot Group, locate the Data section.
- 3 From the Time (s) list, choose 0.
- 4 In the Volume Fraction of Fluid I (Is) toolbar, click I Plot. Repeat the last two steps for the time values 0.08 0.12, 0.16, 0.20, 0.26, and 0.32 s.

Volume Fraction of Fluid I (Is) I

Add a slice plot of the velocity magnitude to the axisymmetric model revolved into 3D.

Slice 1

- I In the Model Builder window, expand the Results>Velocity, 3D (spf) node.
- 2 Right-click Volume Fraction of Fluid I (Is) I and choose Slice.
- 3 In the Settings window for Slice, locate the Plane Data section.
- 4 From the Plane list, choose zx-planes.
- 5 In the Planes text field, type 1.
- 6 Locate the Coloring and Style section. Click Change Color Table.
- 7 In the Color Table dialog box, select Aurora>JupiterAuroraBorealis in the tree.
- 8 Click OK.

Isosurface I

- I In the Model Builder window, click Isosurface I.
- 2 In the Settings window for Isosurface, locate the Coloring and Style section.
- 3 From the Color list, choose Black.

Volume Fraction of Fluid I (Is) I

- I In the Model Builder window, click Volume Fraction of Fluid I (Is) I.
- 2 In the Settings window for 3D Plot Group, locate the Data section.
- 3 From the Time (s) list, choose 0.11.
- 4 In the Volume Fraction of Fluid I (Is) I toolbar, click Plot.

Edge 2D I

- I In the Results toolbar, click More Datasets and choose Edge 2D.
- **2** Select Boundaries 2 and 8–10 only.

Revolution 2D 3

- I In the Results toolbar, click More Datasets and choose Revolution 2D.
- 2 In the Settings window for Revolution 2D, locate the Data section.
- 3 From the Dataset list, choose Edge 2D 1.
- 4 Click to expand the Revolution Layers section. In the Revolution angle text field, type 180.

Surface I

- I Right-click Volume Fraction of Fluid I (Is) I and choose Surface.
- 2 In the Settings window for Surface, locate the Data section.
- 3 From the Dataset list, choose Revolution 2D 3.
- 4 Locate the Coloring and Style section. From the Coloring list, choose Uniform.
- 5 From the Color list, choose Gray.

Finally, create a movie using the current plot group.

Animation I

- I In the Volume Fraction of Fluid I (Is) I toolbar, click Animation and choose Player.
- 2 Click the Play button in the Graphics toolbar.